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17. LIMITATION

**OF ABSTRACT** 

Α

18. NUMBER

OF PAGES

16. SECURITY CLASSIFICATION OF:

a. REPORT

Unclassified

b. ABSTRACT

Unclassified

c. THIS PAGE

Unclassified

Standard Form 298 (Rev. 8-98) Prescribed by ANSI Std. 239.18

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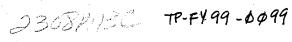
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**PERSON** 



MEMORANDUM FOR PRR (Contractor/In-House Publication)

FROM: PROI (TI) (STINFO)

18 May 1999

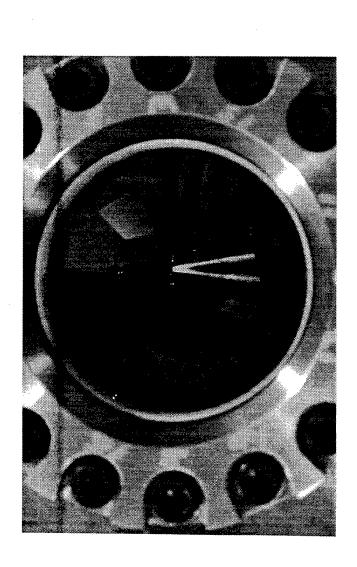
SUBJECT: Authorization for Release of Technical Information, Control Number: AFRL-PR-ED-TP-FY99-0099 Doug Talley, "Basic Research in Liquid Rocket Combustion at the Air Force Research Laboratory" International presentation

(Statement A)

### LIQUID ROCKET COMBUSTION CHAMBER FLOW DYNAMICS RESEARCH STATUS AND PERSPECTIVES IN INTERNATIONAL WORKSHOP ON



### **Basic Research in Liquid Rocket** Combustion at the Air Force Research Laboratory



Doug Talley
Propulsion Sciences
and Advanced
Concepts Division

27-28 May 1999

### GOALS Integrated High Payoff Rocket Propulsion Technology Program (IHPRPT)

<b>Boost and Orbit Transfer Propulsion</b>	2000	2002	2010
<ul> <li>Reduce Stage Failure Rate</li> </ul>	25%	20%	<b>12%</b>
<ul> <li>Improve Mass Fraction (Solids)</li> </ul>	15%	<b>25%</b>	32%
Improve ISP (sec)	14	21	<b>5</b> 6
<ul> <li>Reduce Hardware Costs</li> </ul>	15%	<b>25%</b>	35%
Reduce Support Costs	15%	25%	32%
<ul> <li>Improve Thrust to Weight (Liquids)</li> </ul>	30%	<b>%09</b>	100%
<ul> <li>Mean Time Between Removal (Mission Life-Reusable)</li> </ul>	20	40	100

### **Spacecraft Propulsion**

<ul> <li>Improve I<sub>tot</sub>/Mass <sub>(wet)</sub> (Electrostatic/Electromagnetic)</li> <li>Improve Isp (Bipropellant/Solar Thermal)</li> <li>Improve Density-Isp (Monopropellant)</li> </ul>	20%/200% 5%/10% 30%	35%/500% 10%/15% 50%	20%/200% 35%/500% 75%/1250% 5%/10% 10%/15% 20%/20% 30% 50% 70%
<ul> <li>Improve Mass Fraction (Solar Thermal)</li> <li>Tactical Propulsion</li> </ul>	% C C	%c7	% 6 7
<ul> <li>Improve Delivered Energy</li> </ul>	3%	%2	15%
<ul> <li>Improve Mass Fraction (Without TVC/Throttling)</li> </ul>	2%	2%	<b>10%</b>
<ul> <li>Improve Mass Fraction (With TVC/Throttling)</li> </ul>	10%	<b>50%</b>	30%



# Required Injector Characteristics

- Complete combustion in the shortest possible length
- Main injectors:
   performance vs weight tradeoffs
- Preburners/GG's:
  downstream component
  interactions, eg, turbine
  blades, etc
- Acoustically stable
- Chamber modes
- Feed system coupling
- Chamber/wall compatibility
- Heat transfer/cooling
- Oxygen blanching

- Minimize pressure drop
- Throttling
- Ignitable; minimum ignition transients
- Cost, weight
- The "ilities:"
- Reliability
- Maintainability
- Durability

**Manufacturability** 

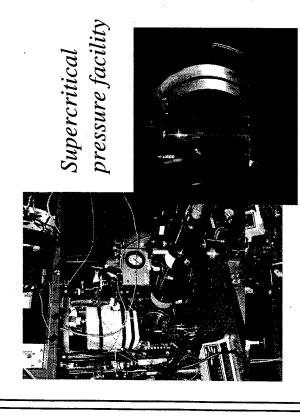
Operability

## Facilities currently supporting basic research

All facilities designed to provide optical access at pressures to 2000 psi (136 atm).

Single element cold flow pressure facility







facility



Max. Fuel sim. press. H,O mass flow rate Max. test art. press. Window Purge gas He mass flow rate N<sub>2</sub> mass flow rate Liquid simulant Gas simulants

 $H_2O(1)$ , others  $N_2(g)$ , He(g)

.20 lbm/s (.09 Kg/s)  $N_2(g)$ , He(g)

.20 lbm/s (.09 Kg/s)

4.0 lbm/s (1.8 Kg/s) 2000 psi (136 atm)

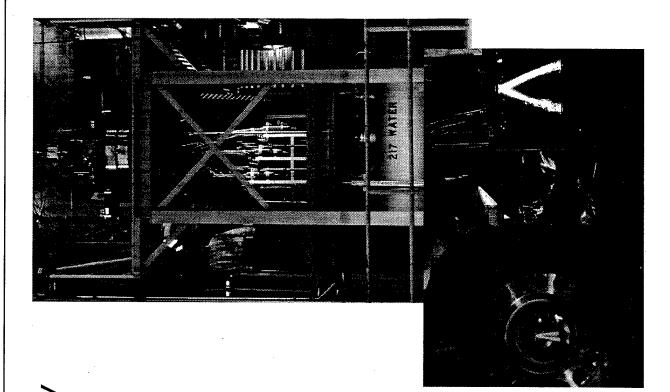
3000 psi. (204 atm)

3000 psi. (204 atm)

Max. Ox sim. press.

axial injector travel and a linear translating Windowed test chamber with 5.5" (14 cm) of injector stage with 5" (13 cm) total radial travel inside chamber, Ability to simulate manifold cross velocities to 30 ft/s (9.1 m/s).

Phase Doppler, Malvern, other diagnostics 27 tube traversable mechanical patternator





### Subscale hot fire facility

Fuel
Oxidizer
Purge gas
H2 mass flow rate
CH4 mass flow rate
O2 mass flow rate
N2 mass flow rate
N2 mass flow rate
Water flow rate

Water system press.

H2(g), CH4(g)
02(g)
N2(g), He(g)
15 lbm/s (.07 Kg/s)
v rate
25 lbm/s (.11 Kg/s)
rate
1.0 lbm/s (.45 Kg/s)
rate
5 lbm/s (.23 Kg/s)

16 lbm/s (7 Kg/s) 2640 psi. (179 atm)

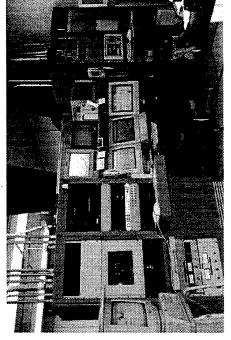


16 ch, 2 MHz per ch A/D, independently controlled Central laser/optics room

128 ch, 200 kbs scanning A/D

<u>Installing in 1999</u> 2000 psi liquid hydrocarbon capability

2000 LOX capability





## Supercritical pressure facility

Chamber Optical access

Stainless
2 facing sapphire
13 cm dia windows

2 facing slot-shaped quartz (12 x 1.3 cm)

2000 psi (136 atm) 473 K

Max chamb. press.

Chamb. temp.

Injected fluid

O2, N2, HC, and mixtures

N2, He, and mixtures

Ambient fluid

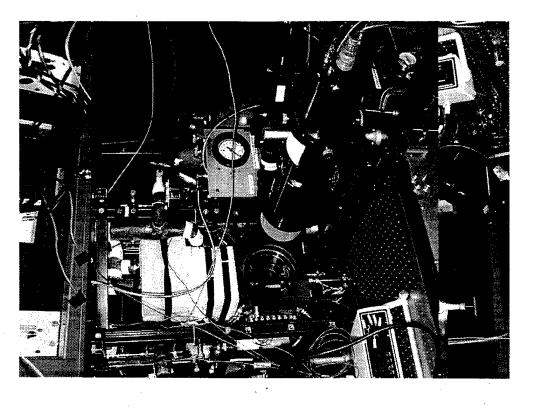
Injected mass flow rate 400 mg/s

Cryogenic cooler

85 K

up to 10,000 SLPM

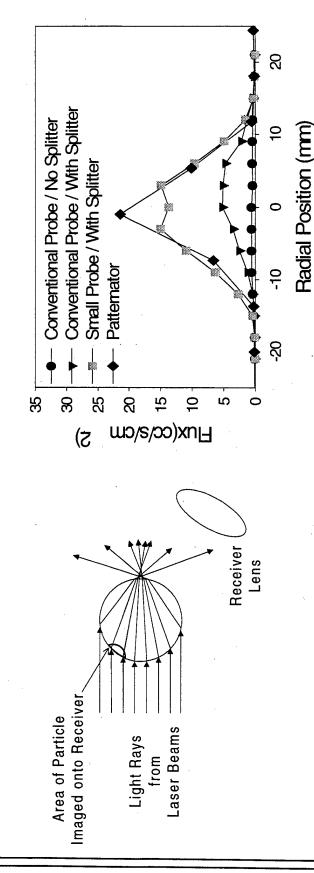
Mass flow meters



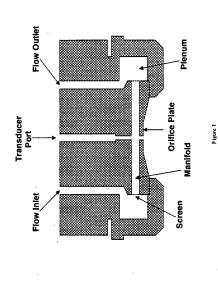


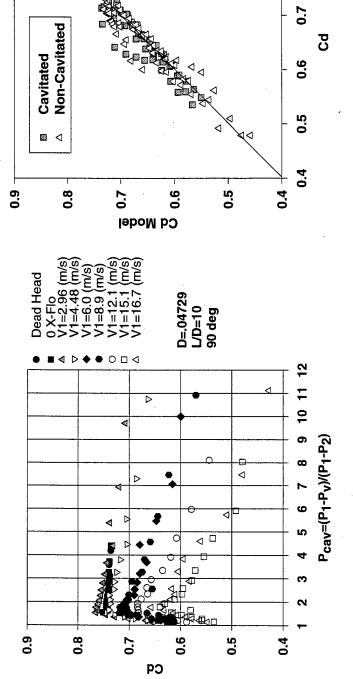
## Dense Spray Diagnostics

- Goal Extend existing diagnostic techniques into the dense spray regime where N  $> 10^5$  cc<sup>-1</sup>.
- The combination of a small probe volume and a flow splitter resulted in a dramatic improvement in PDPA volume flux measurements in a dense spray.



### Effect of Crossflow on Orifice Discharge Coefficients





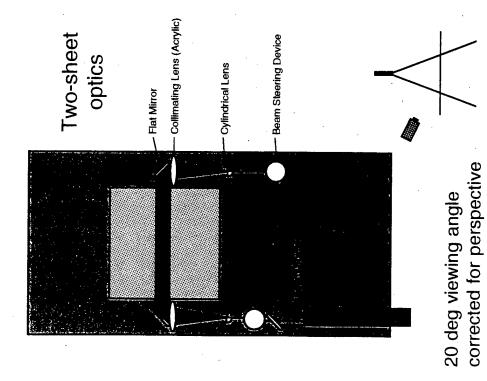
D=1.19 mm, L/D=10, P<sub>1</sub>=.69 MPa

6.0

0.8

# Phillips Laboratory

# TWO SHEET CORRECTION FOR LASER EXTINCTION



Camera response\*

$$G = KI\rho$$

Along a ray,

$$\frac{dG_l}{G_l} = \frac{dl_l}{l_l} + \frac{d\rho}{\rho}$$

$$\frac{dG_r}{G} = \frac{dl_r}{l} + \frac{d\rho}{\rho}$$

Beer's law scattering is the same in both directions at any dx. Thus

$$dI_l/I_l = -dI_r/I_r$$

Adding,

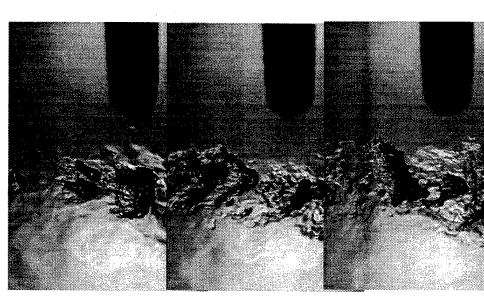
$$\frac{dG_l}{G_l} + \frac{dG_r}{G_r} = 2\frac{d\rho}{\rho}$$

*Independent* of laser sheet intensity.

 $<sup>^*</sup>G$  is gray level, I is laser sheet intensity, ho is spray mass density, and K is a constant



# High Pressure and Supercritical Combustion



Transcritical Oxygen Drops in Nitrogen

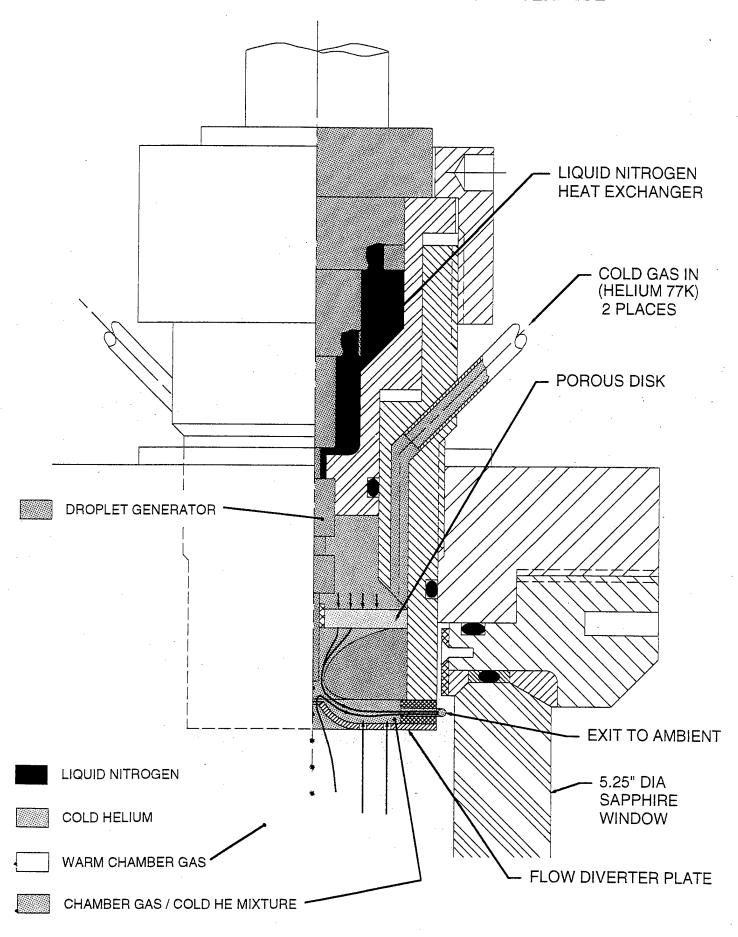
### OBJECTIVE

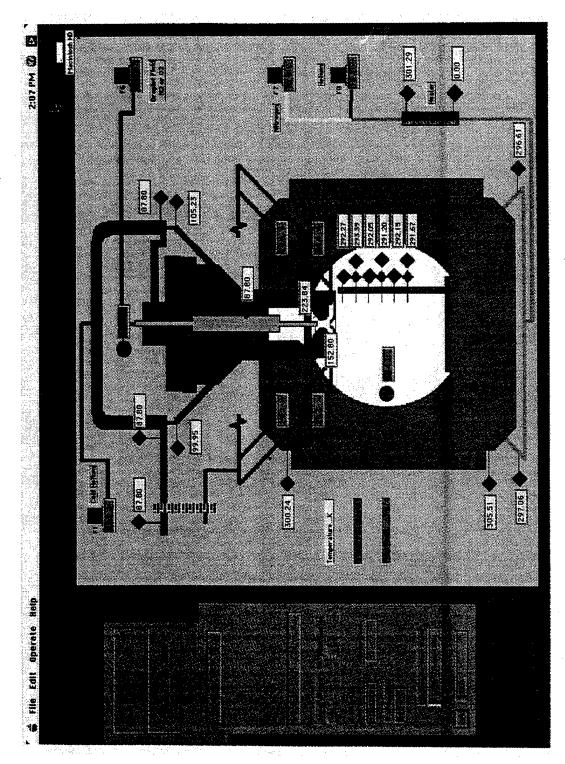
Determine the mechanisms which control the breakup, transport, mixing, and combustion of high pressure and supercritical droplets, jets, and sprays.

### **APPROACH**

- Working fluids include cryogenics
- LOX, LN2
- Droplet studies use free droplets to allow realistic deformation and breakup
- Shadowgraph, Schlieren, and planar Raman visualization of concentrations
- PDPA, Malvern for subcrititical cases
- •Counter dense sprays/distortions by reducing optical path lengths.

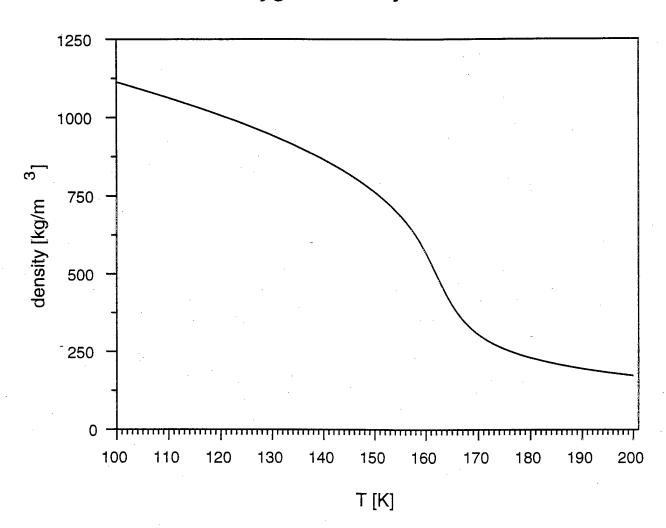
### PRESSURE VESSEL / DROPLET GENERATOR INTERFACE







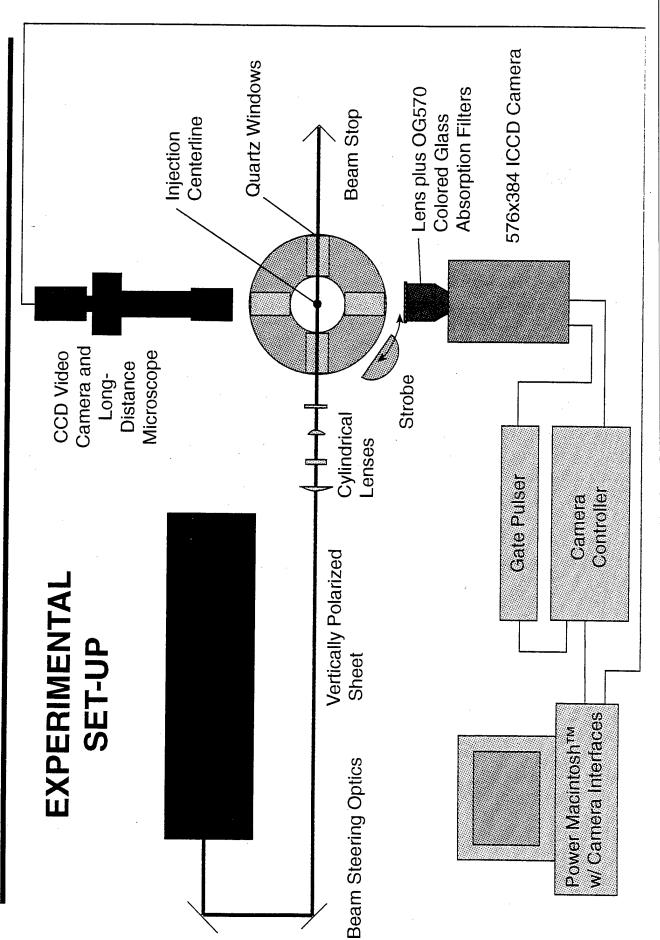
### Oxygen Density at 69 atm





## TRANSCRITICAL PROPELLANT INJECTION EXPERIMENTS







# SUPERCRITICAL DROPLET BEHAVIOR

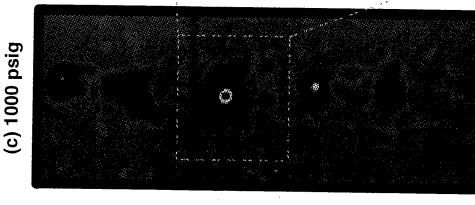


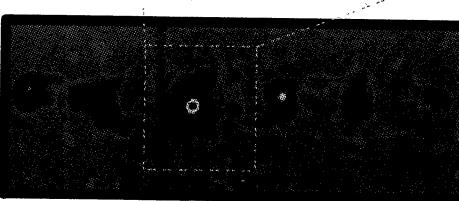
## LOX DROPLETS INTO HELIUM

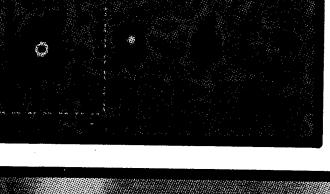


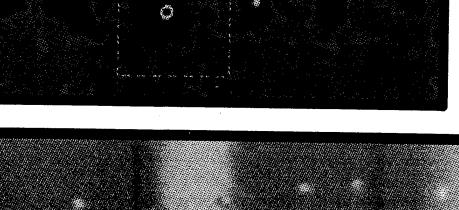
(a) and (b): Photographs indicate effect of pressure

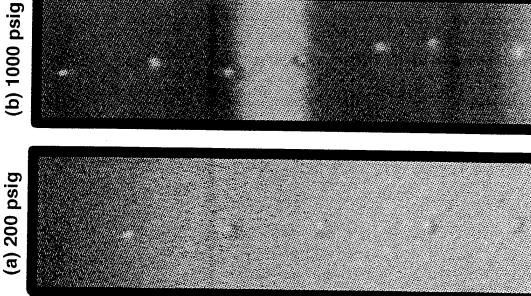
(c): Raman imaging shows non-uniform distribution of vaporized oxygen

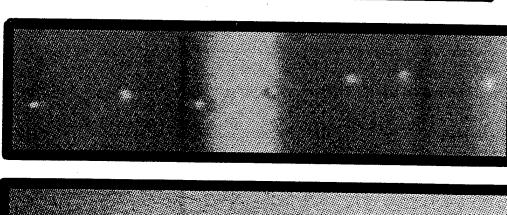












## TOTEL SEATON STATES

## Conceptual Representation of Experimental Results

Pure GO2 or GN2

 $P_r > 1$ ,  $T_r < 1$  or  $T_r > 1$ 

Chilled He

O2 or N2 cloud (may or may not exist)

He cloud (may or may not exist)

Room temperature N2 or He (variable direction and velocity)

.010" filament (size ref.) located behind stream (not always visible)

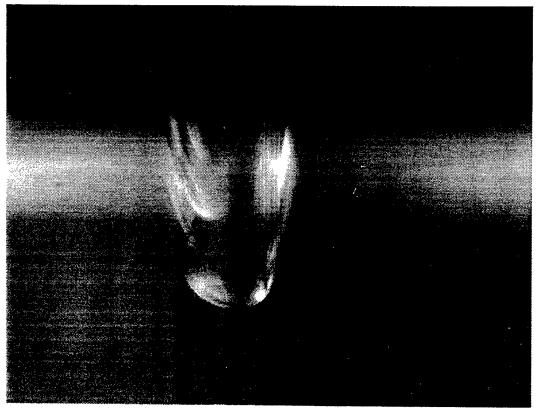
1/16" Thermocouples(6 positions, 1 cm spacing, not always visible)

Drop or jet stream

Supercritical Combustion

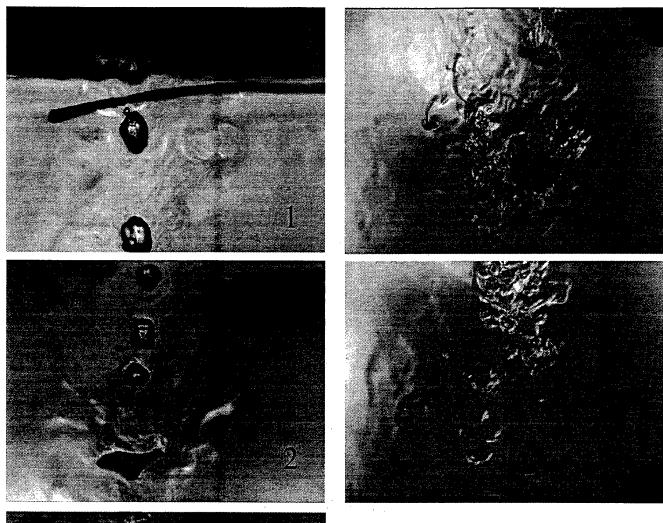
### EXPERIMENTAL RESULTS: **Droplets**





Supercritical Oxygen Drip through He into N2 @ 1100 psig

### Transcritical Injection of Liquid Oxygen Droplets

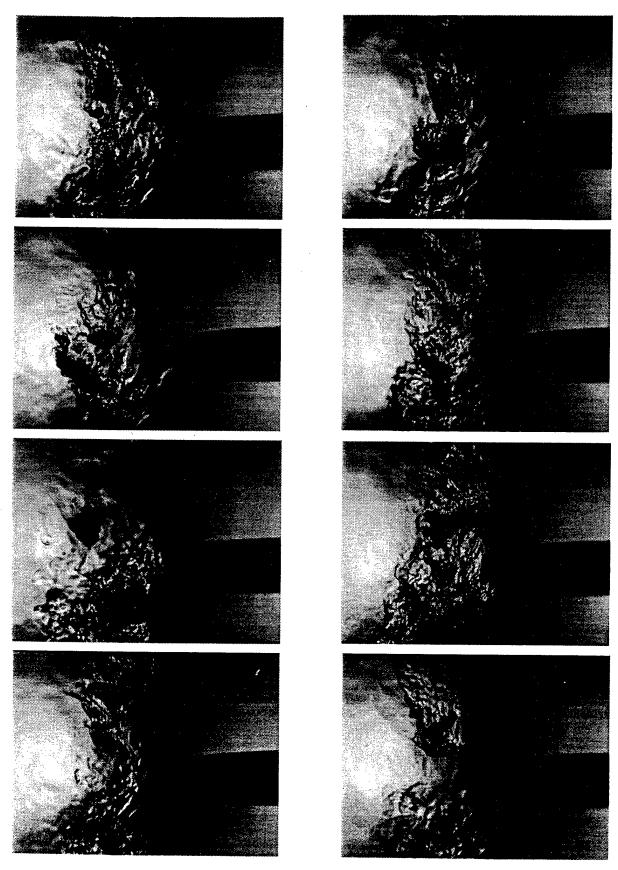




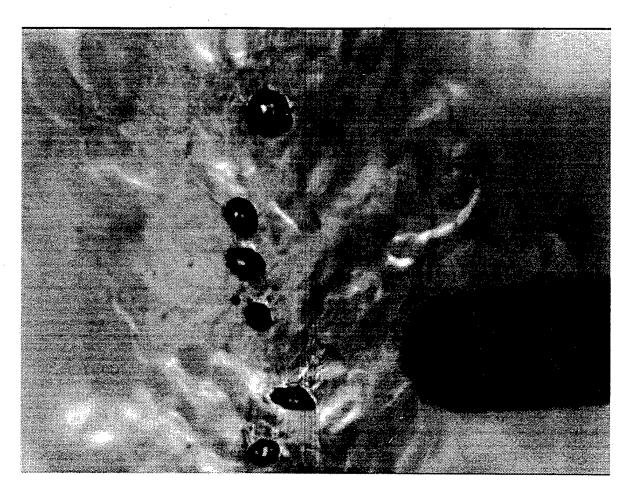
Ambient: N2 @ 970 psig,290K. O2 Injector Temperature: 177K.

Drops formed in chilled helium, nitrogen flowing across stream.

Sequence corresponds to increasing distance downstream.



Transcritical Oxygen Drops in N2 @ 970 psig



Oxygen Droplets Formed in He and Falling into N2 @ 1000 psig, 280K



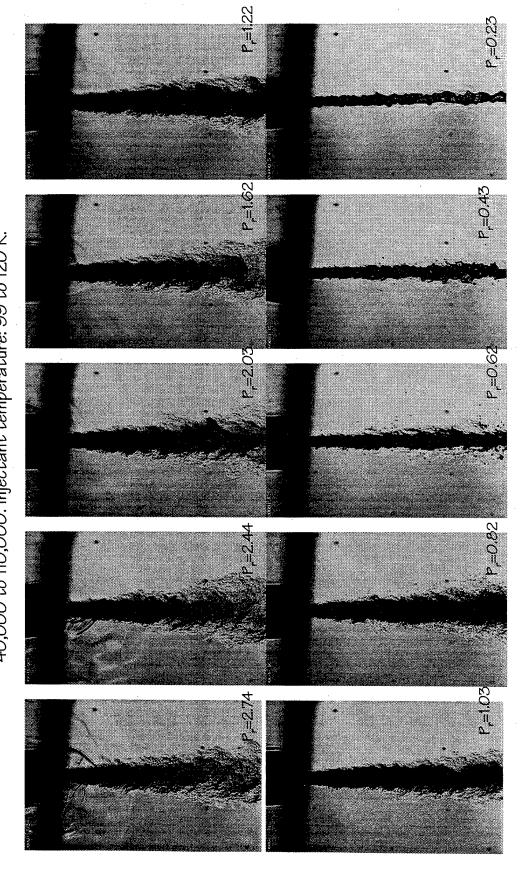
Oxygen Droplet Condensation in Helium @ 1000 psig, 280K

# EXPERIMENTAL RESULTS:





Estx corporation  $N_2 into N_2$  Back-illuminated images of nitrogen injected into nitrogen at a fixed supercritical temperature of 300 K but varying sub- to supercritical pressures. P=P c/P critical Re= 25,000 to 75,000. Injection velocity: 10-15 m/s. Froud number: 40,000 to 110,000. Injectant temperature: 99 to 120 K.

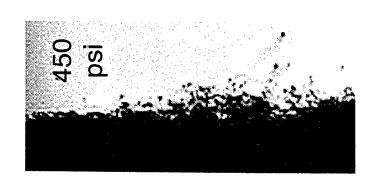




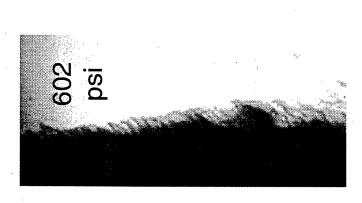
### PRESSURE DEPENDENT MIXING LAYER STRUCTURE

# Nitrogen/nitrogen system ( $P_{cr} = 493 \text{ psi}$ , $T_{cr} = 126 \text{ K}$ )

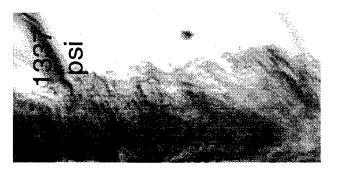
 $T_{inj} = 128 \text{ K}$ ,  $T_{amb} = 300 \text{ K}$ , mass flow = 350 mg/s



Low Pres. Subcritical Droplets



Mod. Pres. Supercritical Ligaments



High Pres. Supercritical Gas layers

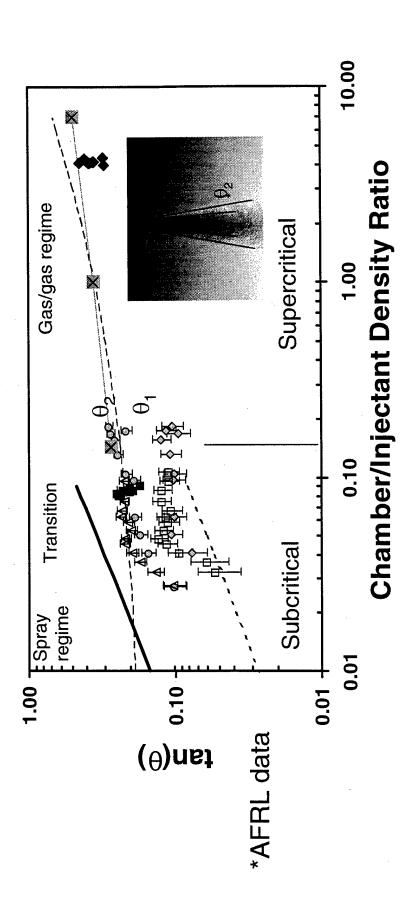
### Sub- and Super-critical Mixing Layer Physics Air Force Research Laboratory -(6.1)

- N2 jet into N2 L/D=200 (\*) Steady Diesel-Type Spray L/D=4 - - - - Steady Diesel-Type Spray L/D=85
- ♦ Cold He jet into N2; L/D=200 (\*)
- ) Cold N2 jet into He; L/D=200 (\*)

N2 jet into N2 Darkcore (\*)

- △ O2 jet into N2; L/D=200 (\*)
- □ O2 jet into N2; Darkcore (\*)

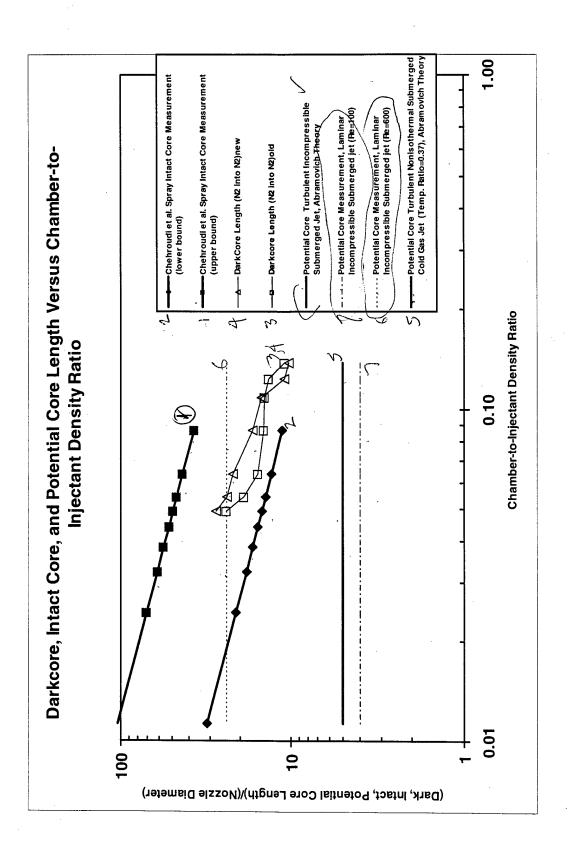
--- Theory (Papamoschou&Roshko)







### Jet Dark Core Length



### Characteristic Times

- et al.):  $(\rho_l L^3/\sigma)^{1/2}$  ;  $\rho_l$  , L ,  $\sigma$  are liquid density, characteristic dimension Characteristic bulge formation time  $( au_b)$  at the jet interface (Tseng of turbulent eddy, and surface tension, respectively.
- Characteristic time for gasification  $(\tau_a)$  (D-square law):  $D^2/K$ ; D and Kare drop diameter and vaporization constant.
- may not be separated as an unattached entity (onset of the gas-jet appropriate length scales) are comparable then an interface bulge A Hypothesis: If these two characteristic times (calculated for behavior at supercritical condition)

## Similar equation format for different

### cases

Sommerfeld equation and stability analysis to find the wavelength of Theoretical isothermal liquid spray growth rate  $( heta_s)$  based on Orrthe most unstable interface wave:

$$\theta_s \equiv 0.27 \left[ O + (\rho_q/\rho_l)^{0.5} \right]$$

Papamoschou/Rashko theory for incompressible variable-density gaseous mixing layer/jet:

$$\theta_{P/R} \equiv 0.17 \left[ 1 + (\rho_g/\rho_I)^{0.5} \right]$$

Dimotakis theory for incompressible variable-density gaseous mixing layer/jet:

$$\theta_D = 0.212 [0.59 + (\rho_a/\rho_I)^{0.5}]$$

ALL HAVE THE SQUARE ROOT OF DENSITY RATIO AND THE SAME EQUATION FORMAT

## Proposed "intuitive/smart" equation

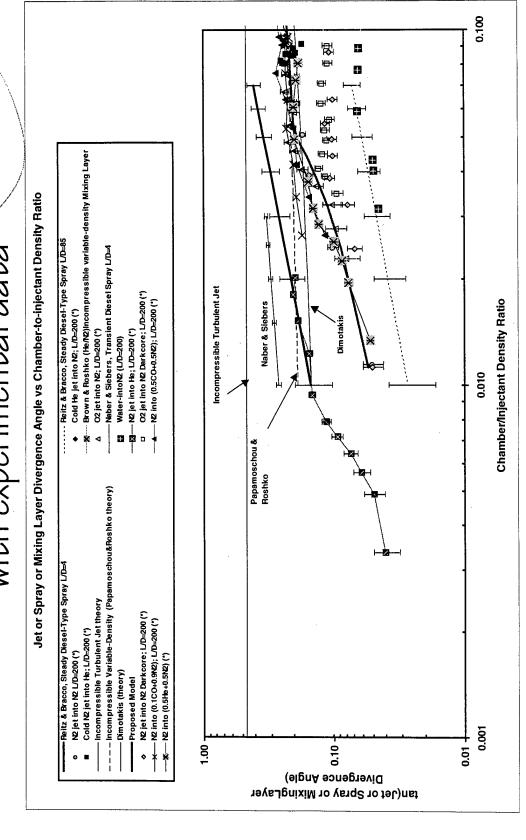
"intuitive/smart" equation is proposed for both sub- and supercritical Based of the information of the previous slide the following measured growth rates:

$$\Theta_{Ch} \equiv O.27 \left[ \left( \tau_b / (\tau_b + \tau_g) \right) + \left( \rho_g / \rho_l \right)^{O.5} \right]^{-1}$$

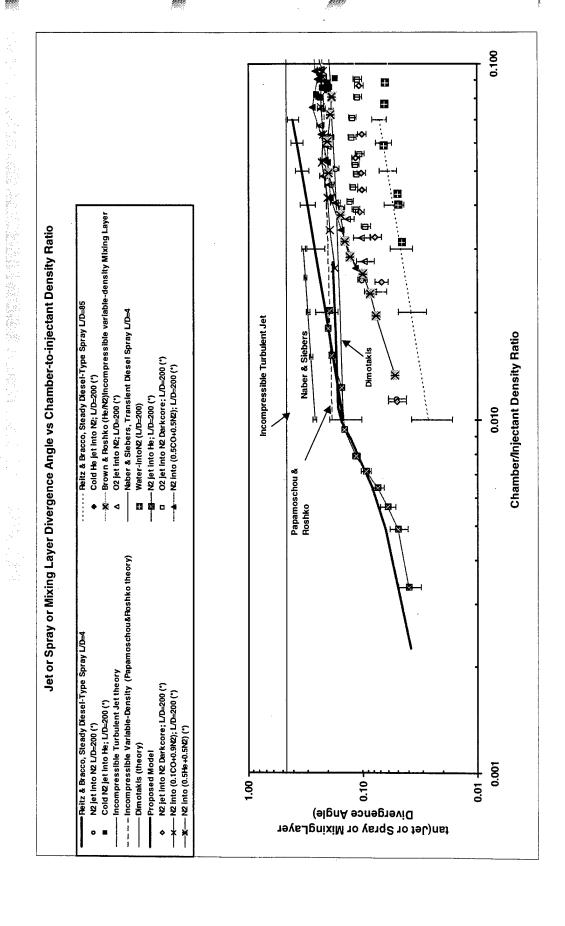
Note

- For isothermal liquid case:  $\tau_g >> \tau_b$  and  $\tau_g \to \infty$ . It then collapses to the isothermal spray case.
- After that it is maintained constant at 0.5n for supercritical jet. The transition point is found to be approximately when  $(\mathbf{\tau}_b/(\mathbf{\tau}_b+\mathbf{\tau}_a))\equiv 0.5.$ For subcritical the  $( au_b/( au_b+ au_g))$  is calculated until it reaches 0.5.
- Only a horizontal axis variable transformation is needed to fit with the N<sub>2</sub>-into-He experimental growth rate data.

### Comparison of the proposed equation (solid red line) with experimental data



### equation with the N<sub>2</sub>-into-He experimental data Comparison of the proposed "intuitive/smart"





## FRACTAL DIMENSION vs. RELATIVE PRESSURE

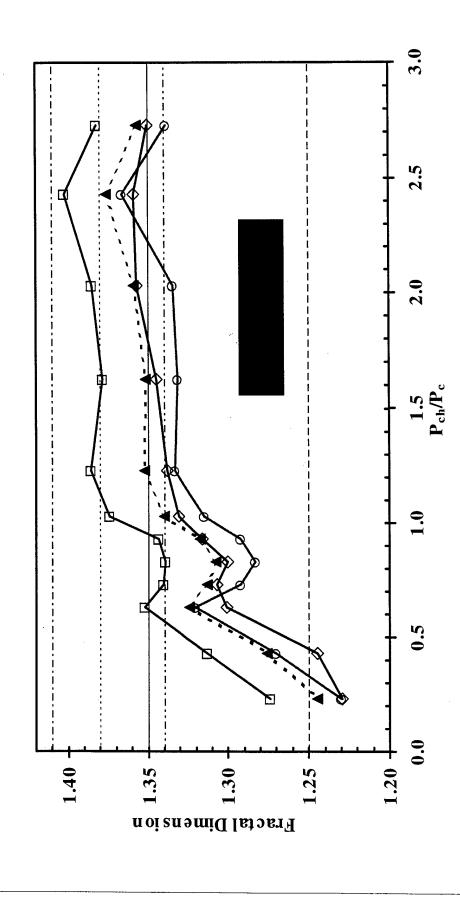
	(SN)
32 (N2into N2)	- AVERAGE (N2into N2)
BOX32	AVERA
•	1

-Sreenivasan & Meneveau (axisymmetric gaseous jet)

---- Taylor & Hoyt (2nd-wind-induced water jet breakup)

---- Dimotakis et al. (turbulent water jet)

...... Sreenivasan & Meneveau (gaseous boundary layer)

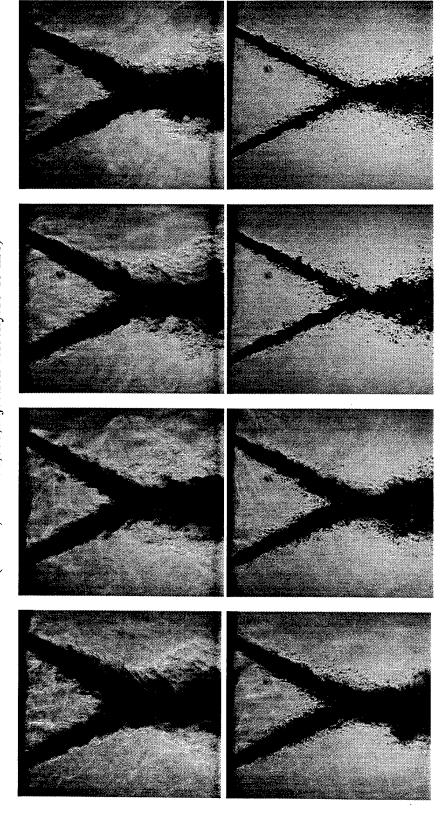


# Instant images of Sub- and Supercritical impinging jets

 $N_2 \text{ into } N_2$ ( $P_{critical} = 3.39 \text{ MPa}; T_c = 126.2 \text{ K}$ )

 $(P_{ch} = 800, 600, 500, 400, 350, 300, 200, 100 psig;$  from upper left to lower right)  $(P_{ch} = 5.5, 4.2, 3.5, 2.8, 2.5, 2.1, 1.5, 0.8 MPa;$  from upper left to lower right)

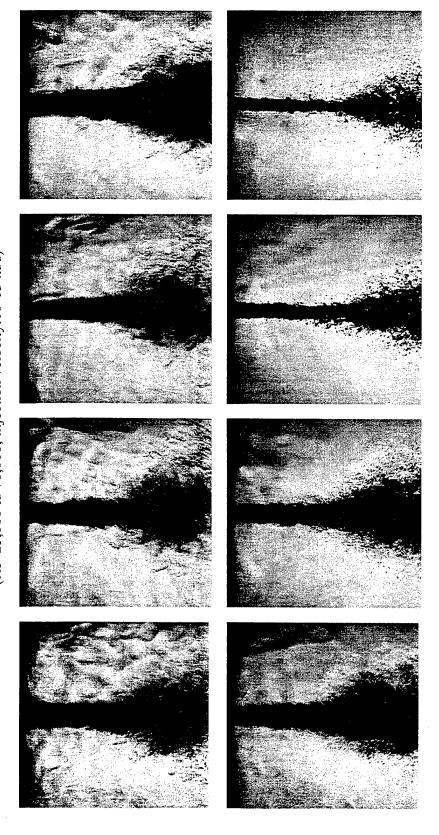
(Re=25,000 to 70,000; injection velocity:10-15 m/s)



# Instant images of Sub- and Supercritical impinging jets

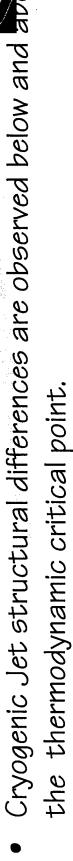
 $N_2 \; into \; N_2 \\ (P_{critical} = 3.39 \; MPa; \; T_c = 126.2 \; K) \\ (P_{clh} = 800, 600, 500, 400, 350, 300, 200, 100 \; psig; \; from \; upper \; left \; to \; lower \; right) \\ (P_{clh} = 5.5, 4.2, 3.5, 2.8, 2.5, 2.1, 1.5, 0.8 \; MPa; \; from \; upper \; left \; to \; lower \; right)$ 

(Re=25,000 to 70,000; injection velocity:10-15 m/s)





### Summary and Conclusions



Liquid-Jet like appearance up to near critical point similar to second wind-induced liquid jet breakup regime. Gas-jet like appearance above the critical point. No drops are observed.

A unique plot has been constructed for the jet growth rate covering density ratio range of up to a 1000.

incompressible variable-density turbulent gaseous mixing layer. Measured growth rate (divergence angle) of our cryogenic jet under supercritical condition agrees well with the theoretical equations by Papamoschou & Roshko and Dimotakis for methal





## Summary and Conclusions (cont.)

- vanishingly small surface tension and heat of vaporization. Transition to full atomization regime is inhibited due to
- the critical point of the injectant. Here the gas-jet like behavior is All tend to strengthen the position that jets under the condition investigated here exhibit gas-jet like behavior at near and above quantitatively demonstrated and verified for the first time.
- vaporization/combustion results under the conditions where gas-The relevancy of current injection models and some drop jet like behavior is detected should be reexamined.

# Basic Research Opportunities

### 1990's at AFRL

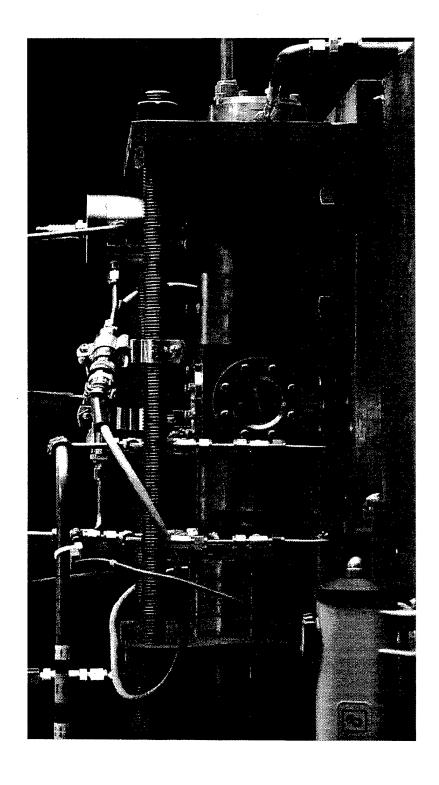
- High pressures, "steady."
- Gas/gas injection

### Future

- Injector/chamber interactions
- Transients
- Organized
- Un-organized
- Revolutionary cycles
- Pulsed detonation propulsion
- Combined cycle



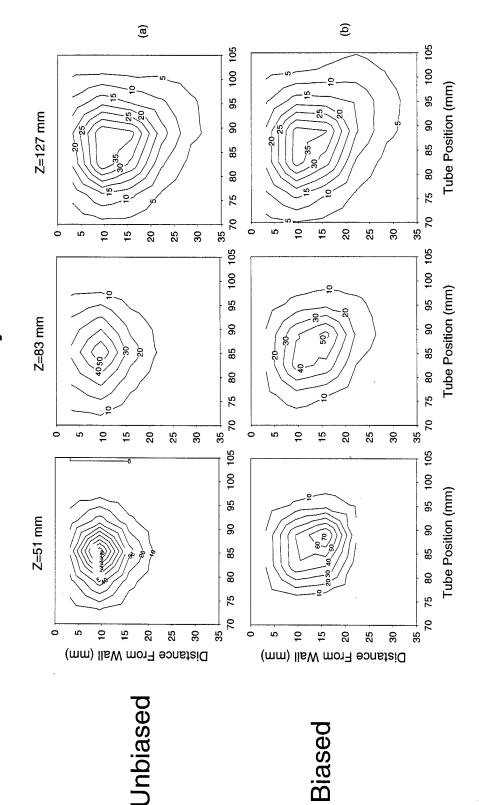
### Gas/gas hardware





## LOX post biasing study

### Water/N2, density ratio = 117





# Pulsed Detonation Rocket Engine Test at AFRL

